IN THE SPECIFICATION

Please amend the specification as follows:

Please amend paragraph 3 on page 2 as follows:

An example of an HER process is disclosed in USSN 10/083778 (filed on 25th February 2002, now abandoned) and this disclosure is incorporated herein by reference. It is disclosed generally that a cooling stream of reactive diluent fluid may be introduced to a stream of fresh syngas produced in a primary heat-generating unit to produce a cooled mixture of syngas and reactive diluent fluid. The subsequent reaction of at least two of the components of the mixture will either produce further carbon monoxide or gasify solid carbon particles. In particular, in this disclosure hydrocarbon-containing fuel is exothermically reacted with an oxidant gas comprising molecular oxygen in a first reactor to produce an exothermically-generated syngas product. A stream of reactive diluent fluid is combined with a stream of said exothermically-generated syngas product to produce a reactive mixture and the reactive mixture is reacted in a second reactor to produce a reacted syngas product if desired, this reacted syngas may be introduced into the secondary reforming unit in an HER process. The reacted syngas product is cooled before being introduced into the secondary unit thereby avoiding negatively affecting the mechanical integrity of the secondary unit. In the exemplified embodiment, a POX reactor is used in combination with an EHTR.

Please amend paragraph 2 on page 5 as follows:

The production of syngas having a hydrogen to carbon monoxide ratio lower than 2 to 1 is particularly undesirable when using an EHTR coupled to a POX reactor. This example of a disadvantage in prior art processes is discussed in USSN 10/083778, which is now abandoned. It has been found, surprisingly, that when this ratio is below 2 to 1, it is necessary to limit the amount of heat transferred in the EHTR because, when all available carbon dioxide is recycled back to the syngas generation process then, in order to make the required hydrogen to cargon monoxide ratio, the additional reforming which takes place in the EHTR using heat from the POX reactor must be limited since the extra heat would produce mainly hydrogen which is not required in excess. When the syngas ratio is 2 to 1, all of the POX heat can be utilised in the EHTR. The product syngas flow is increased and its exit temperature is lower.